Fuel Ethanol from Sugar Cane Bagasse





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Competence Platform on Energy Crop and Agroforestry Systems for Arid And Semi-Arid Ecosystems

> Puente de Ixtla, Morelos. Wednesday 4, 2009

Outline of the Presentation

- Motivation and the Mexican perspective
- Lignocellulose Biomass
- 2ng Generation Fuel Ethanol
- Carbon metabolism studies in ethanologenic Escherichia coli
- Biomass Sources and Potential
- Final Remarks
- Acknowledgements
- Questions

New fuels are needed to substitute oil derivatives and fossil fuels

Oil

- **✓** Depletion (Mexico ~2020)
- **✓**Price Increase
- **✓** Contamination-Spills
- **✓** Emissions
- **✓** Economic National Support



Oil, natural gas and carbon: Industrial activities, electricity generation, transport, etc.

Alternative Renewable E

Wind

Hydro

Waves

Geothermic

Solar

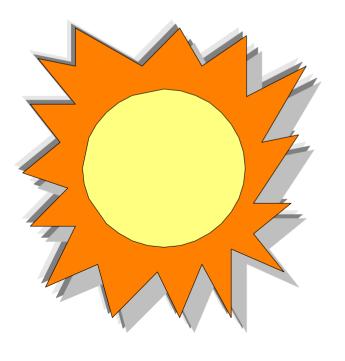
Electricity

Biomass: Solid Bio-fuel

Liquid Bio-fuels
For Transportation
Fuel Ethanol

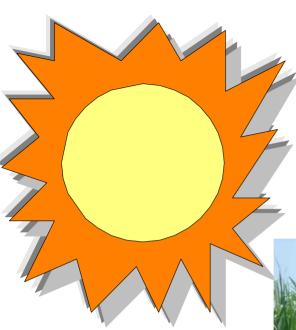
Sun → Biomass → Fossil Fuels

~ 100 Million Years









Sun → Biomass → Bio-Fuels

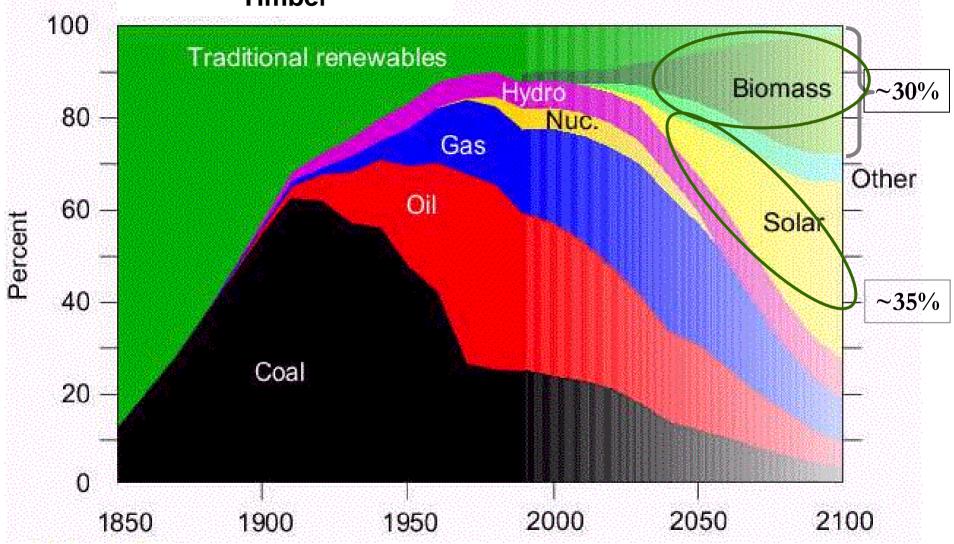
!~ or < 1 Year!





Mexico 2004: 8%
Sugar Cane Bagasse
Timber

Energy Consumption



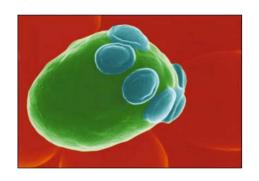
Fuel Ethanol Production

Brazil, expertise 30 years

More than 15,000 million L/year (41 million L/day)

Sucrose syrups from Sugar Cane + Yeast → Ethanol 40% car use E95. Others E22. Ford, GM, WV, Honda, etc.

Saccharomyces cerevisiae









Mature Technology

Fuel Ethanol Production

USA: expertise 20 years

2006: More than 41 million L/day (more than Brazil)

Corn Starch + Amylases → Glucose

Glucose + Yeast → Ethanol

E10 any car: 2% gasoline consumption EUA



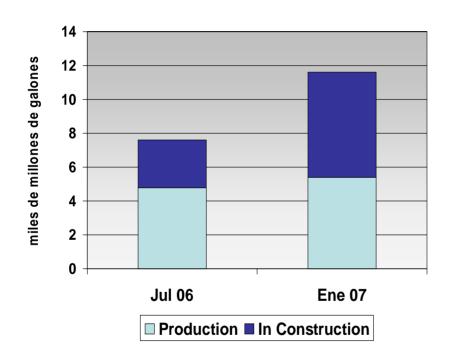






Mature Technology

1st Generation Fuel Ethanol USA and Brazil



Year	Area (Mha)	Alcohol (Mm³)
2005	5.50	15.60
2015	7.92	45.00
2025	8.64	78.00

Colombia

~2 years expertise 1 million liters/day

Sucrose syrups from Sugar Cane + Yeast → Ethanol





What about Mexico?

Mexican Scenario: Fuel Ethanol

- Mexican demonstrated oil reserves will be depleted in 9 years
- 33% of the Mexican federal income is based in oil commercialization.

Gasoline Price 8 - 10 pesos/L

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Glucose \rightarrow 2 Ethanol + 2 CO<sub>2</sub>
Sucrose \rightarrow 4 Ethanol + 4 CO<sub>2</sub>
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Theoretical Yield: 0.51

 $g_{\text{ETHANOL}} / g_{\text{(GLC or SUC)}}$

 $0.64 L_{EtOH}/kg$

Substrate	Bulk Price in Mexico (pesos/kg)	Et-OH Prod. Cost Substrate (pesos/L)
Glucose Sucrose	$\overset{\textstyle \rightarrow}{\rightarrow}$	8-11 8-11

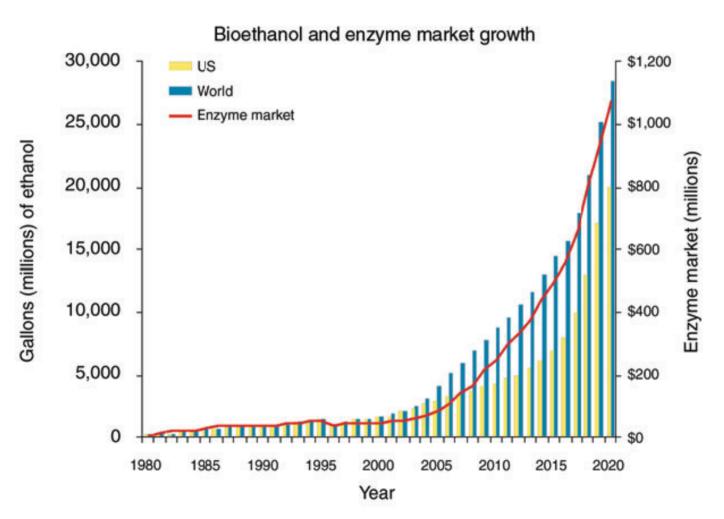
Glucose, Corn Imports: 8 x 10⁶ metric tons & Corn Yield: 2-4 ton/ha vs 12-14 ton/ha Sucrose, small surplus – small market & high sugar cane price (3 times the price of Brazil)

Vision 20 years

 Given that in 20 years the main form of transportation fuel will still be liquid fuel, the technological vision for 2020-30 is that bio-fuels will evolve to those that will integrate seamlessly into current transportation refining to end use fuel systems: Bio-ethanol, bio-diesel and other liquid and gaseous bio-fuels need to be produced

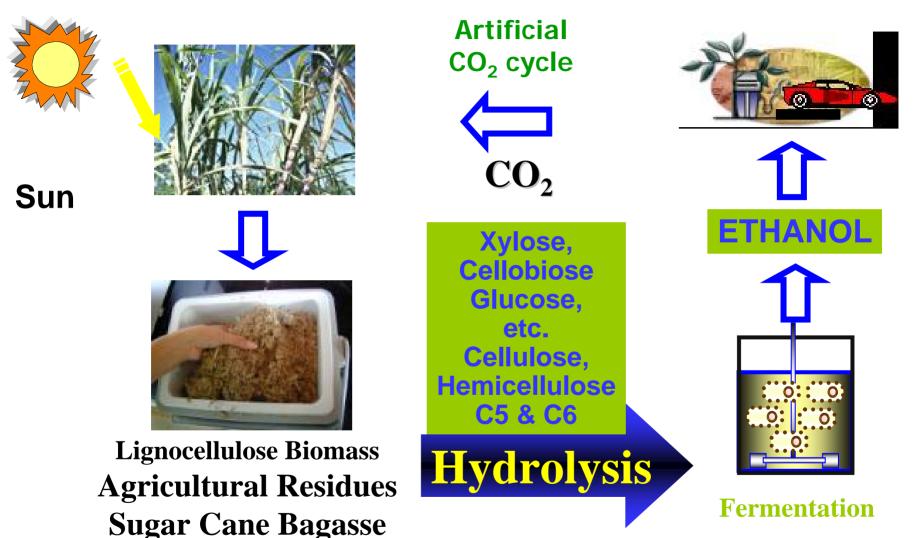
Look for solutions: Biotechnology

Bio-Ethanol Market



Schubert. Nature: 2006

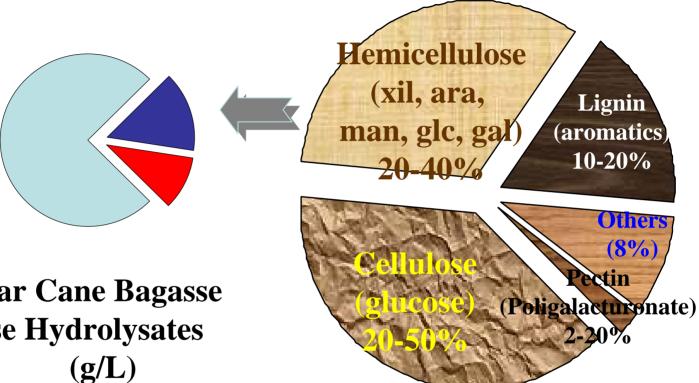
Second Generation Fuel Ethanol



Purpose: Design microorganism and process to transform Lignocellulose (cellulose & hemicellulose: pentoses, hexoses, disaccharides) to ethanol Martinez et al. 2006



Lignocellulose Sugar Cane Bagasse



Sugars in Sugar Cane Bagasse Hemicellulose Hydrolysates

> 80 **Xylose:**

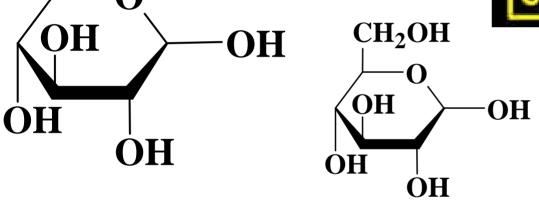
Arabinose:

15 Glucose:

Pentoses 85% + Hexoses 15% + (Gluc+Man+Gal) (Xil + Ara)+ Acetate + Glucuronic Acid

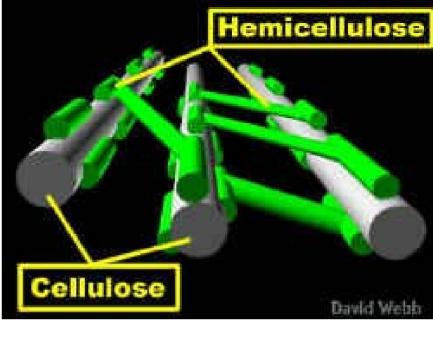
Biomass - Lignocellulose Future Raw Material

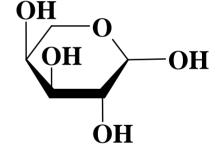
Hemicellulose Hydrolysis Products



Xilose 5-carbons

Glucose 6-carbons





Arabinose 5-carbons

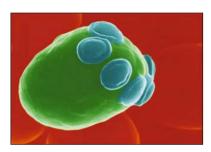
Yeast: Do not Ferment Pentose Sugars

Two main strategies: Pentoses > Ethanol Metabolic Pathway Engineering

A: Ethanol producer

Increase substrate range. Engineer to use pentoses

Saccharomyces cerevisiae and Zyrlomonas mobilis









Hexoses

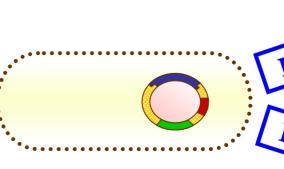
B: NO Ethanol producer

Pathway complementation. Engineer to produce only ethanol

Escherichia coli





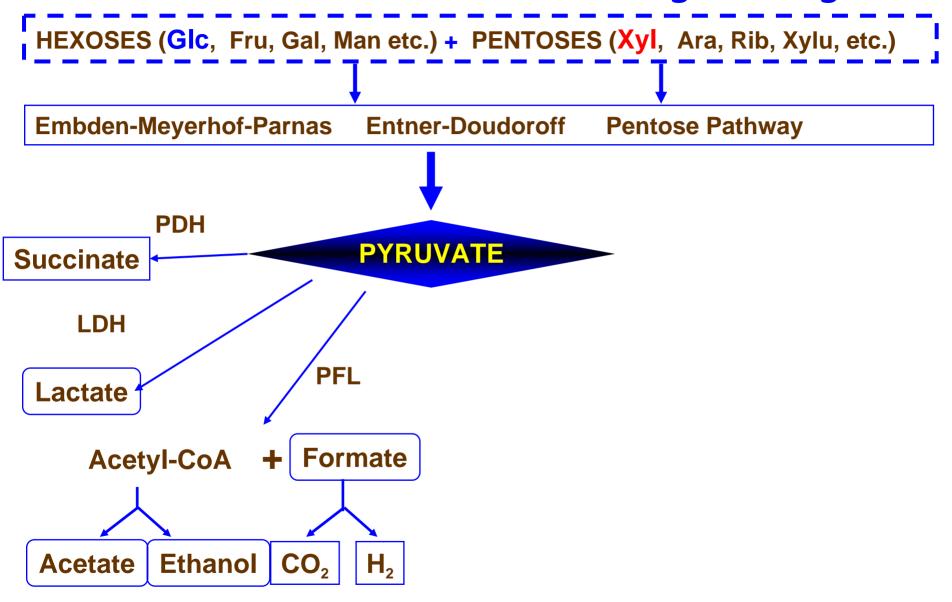




Pentoser

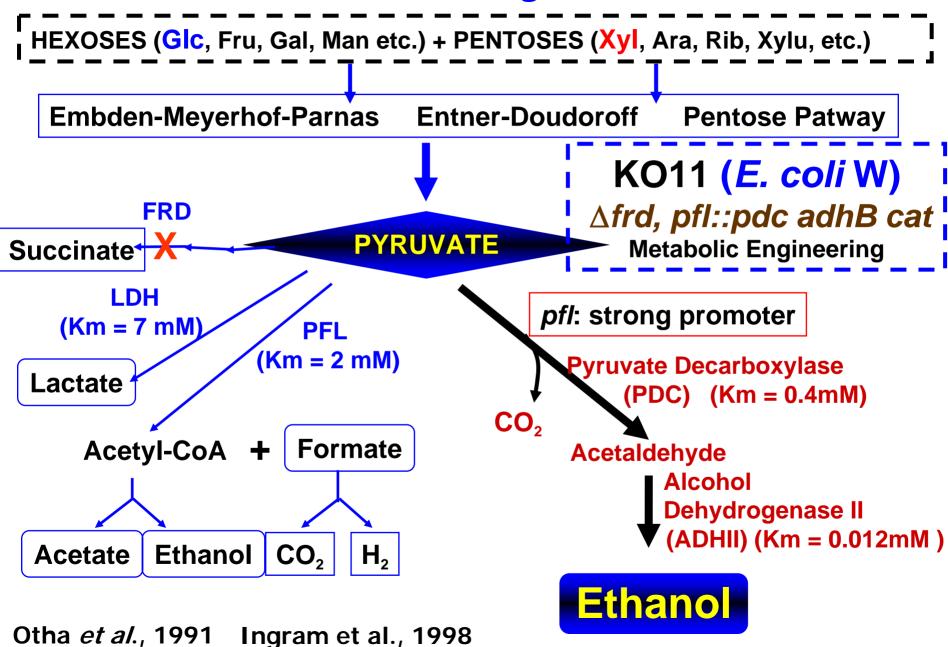
Ethano

Escherichia coli: Uses a wide range of sugars



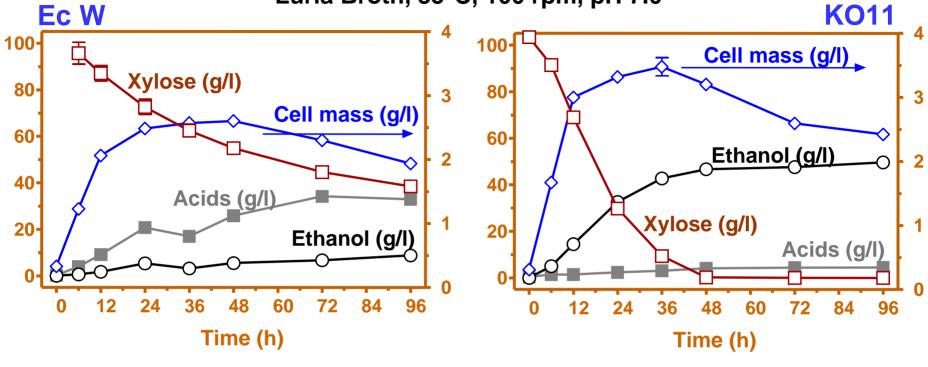
and make fermentation products, but little ethanol

Construction of ethanologenic E. coli: KO11



Xylose (10%) fermentation





Cell mass:

μ:

 q_s : $(g_{XyI}/g_{DCW}h)$ Q_{EtOH} $(g_{Et-OH}/I h)$

Theoretical Yield = $0.51 g_{Et-OH}/g_{Glc or Xyl}$

$$KO11 > Ec_W (34\%)$$

$$KO11 > Ec_W$$
 (30%)

$$KO11 > Ec_w$$
 (30%)

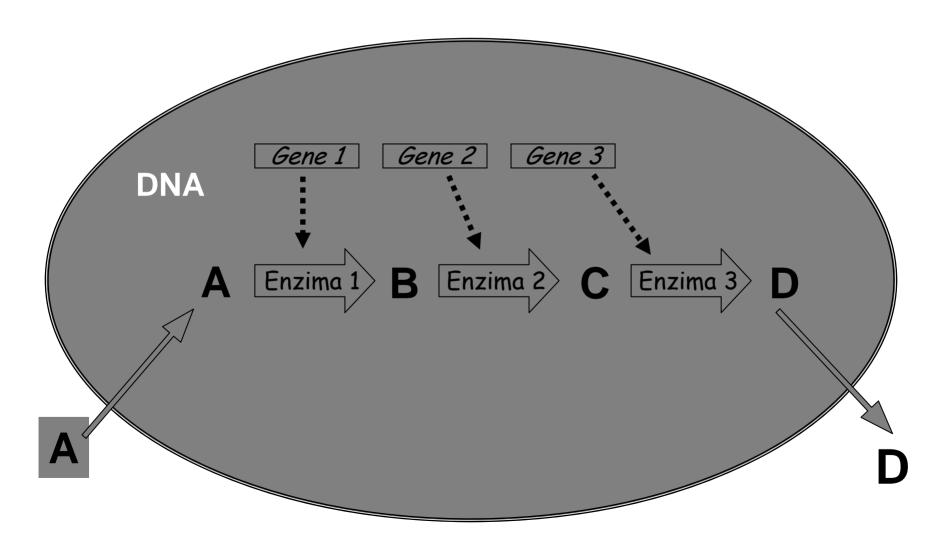
$$KO11 = 1.0$$

Yield

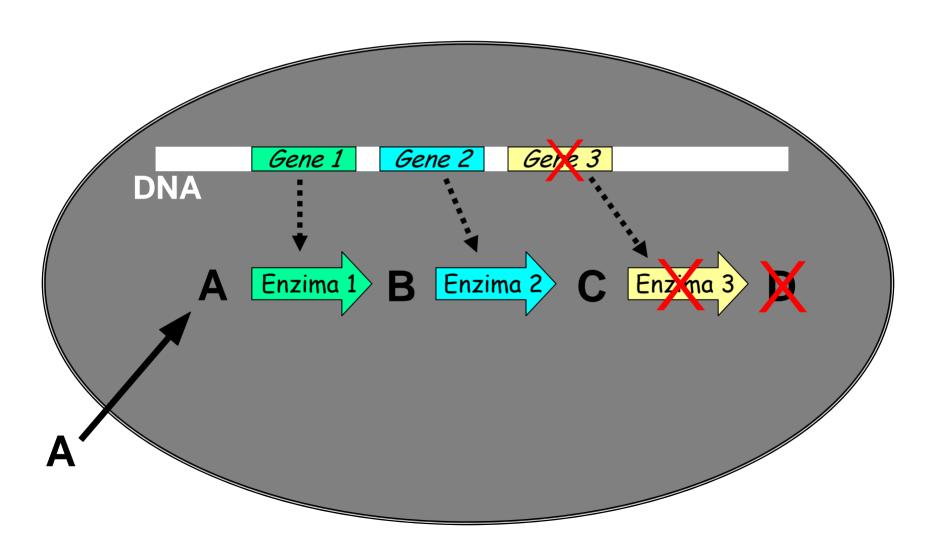
94.0%

Tao et al., 2001, Martínez et al., 1999

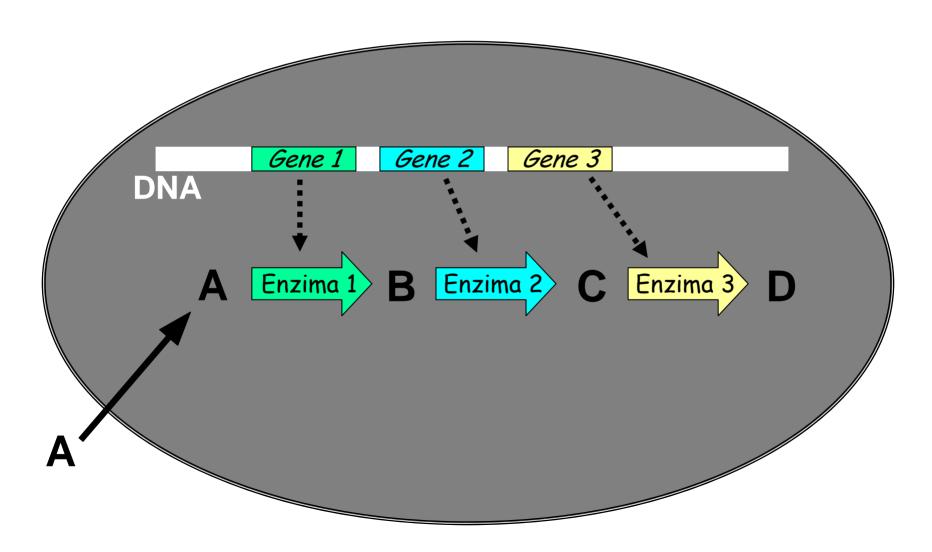
Metabolic Engineering (Genetic Engineering Tools)



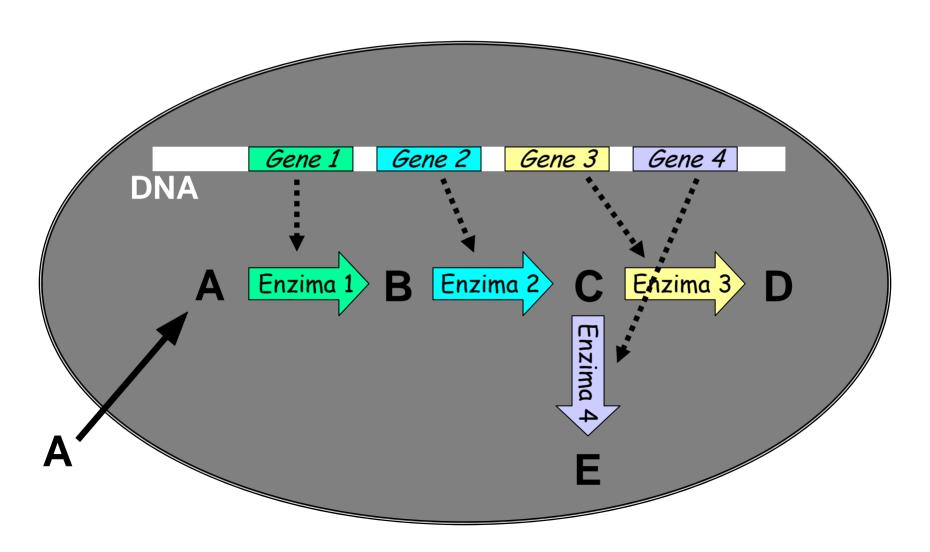
Delete - Interrupt Genes



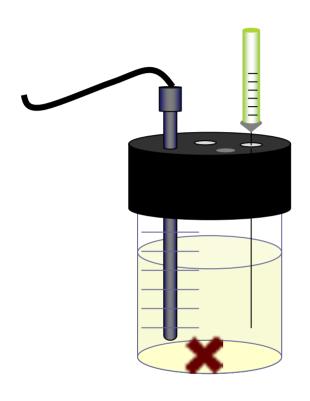
New genes



New (add foreign) genes



Strain evaluation





Fermentor setup: 6-Mini-fermentors (Fleakers)

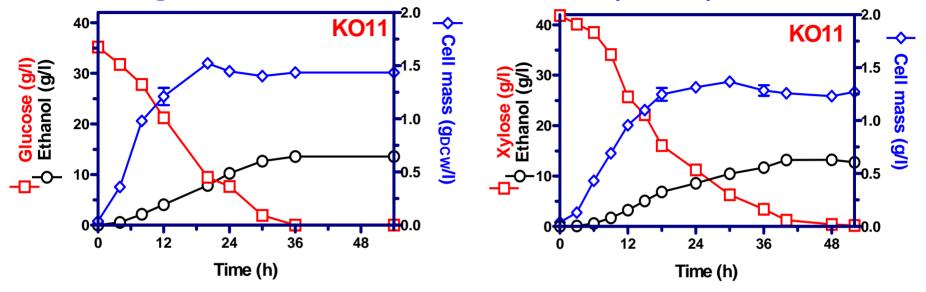
Working volume 200 ml

Mineral media (some with Rich Media) & Sugars (Xyl, Glc)

Temperature: 37°C; Speed: 100 rpm; pH: 7.0

Without aeration

KO11: Glc or Xyl (4%): Mineral Media Sugar Cane Hemicellulose Hydrolyzates



In comparison with rich media, in mineral media there are reductions by: $57_{\rm Glc}~\&~63_{\rm Xyl}~\%$ in cell mass formation; 25% in the specific growth rate $70_{\rm Glc}~\&~60_{\rm Xyl}~\%$ in the specific sugar consumption rate

 Q_{EtOH} is reduced to 0.42_{GIC} & 0.33_{XyI} g_{Et-OH}/I h, for glucose and xylose

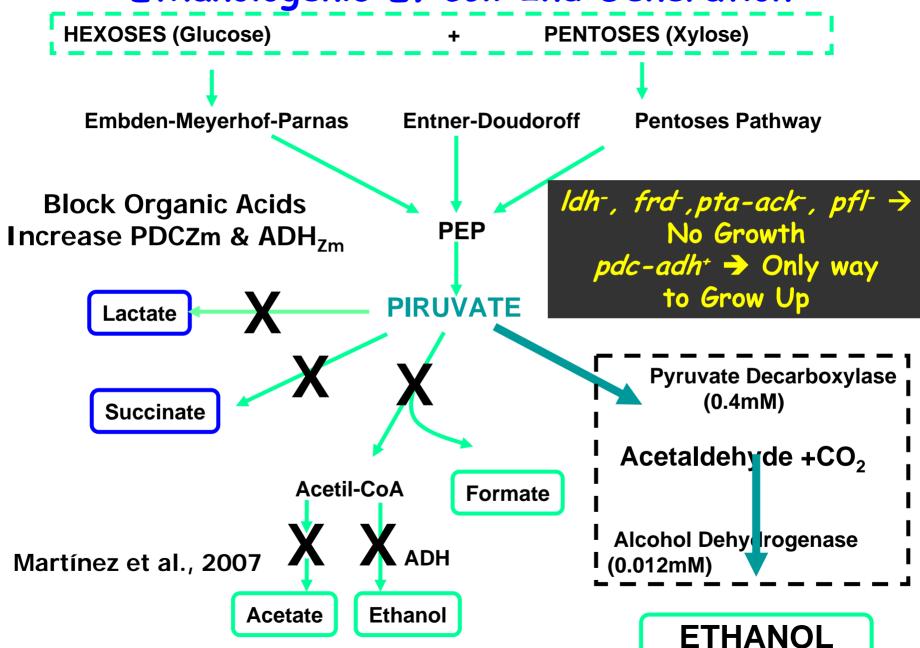
Yield 70%

Yield 60%

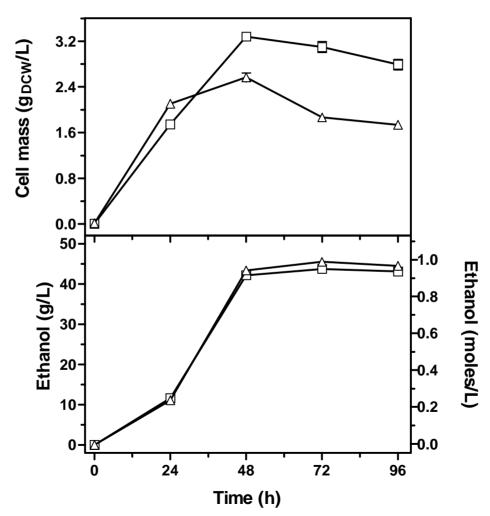
Main Conclusion

 The study provides the basis for the implementation of appropriate genetic modifications to increase the ethanol yield when mineral media or sugar from hemicellulose syrups containing a large amount of pentoses are used, for instance, the disruption of succinate and lactate pathways that compete for ethanol production.

Ethanologenic E. coli 2nd Generation

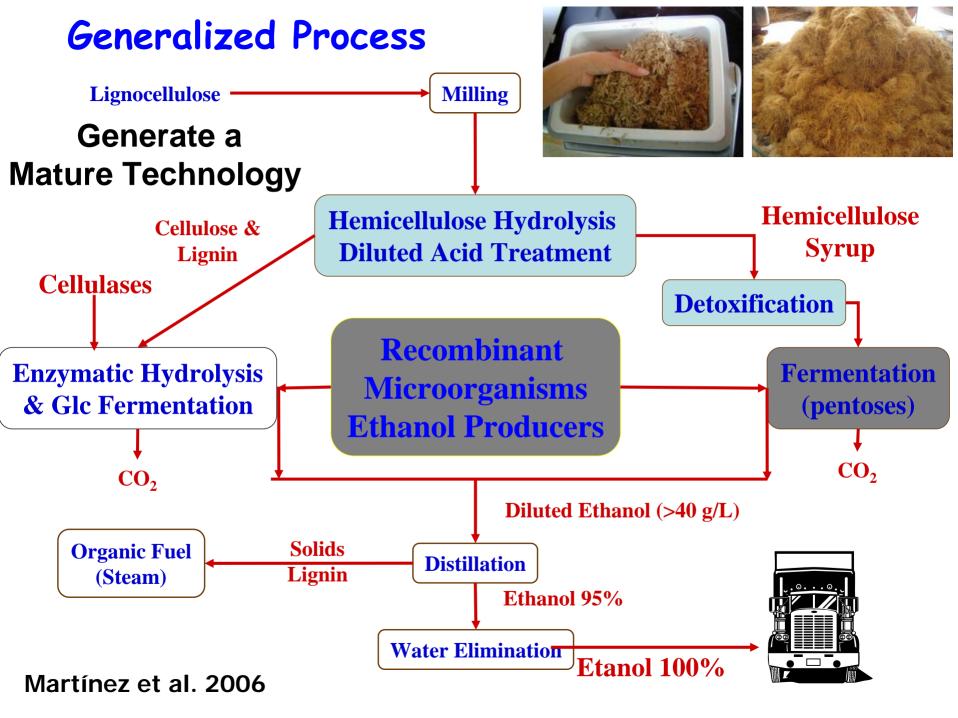


Ethanol Production in Mineral Media-Xyl-Glc Or Hemicellulose Syrups



2nd Generation

- Homo-ethanologenic strains
- Capable to ferment glc, xyl or mixtures (100 g/L total sugars) in 48 h
- Yield above 90% of the theoretical
- Some metabolic evolution work was performed to contend with the effects of pfl interruption.



SCB



Production Potential with Sugar Cane Base 100 Ton/Ha

- Cane syrups: 7,500 L/Ha
- Bagasse (300 kg/Ton, 50% humidity)
- 5,500 L/Ha
- Syrups + Bagasse
- 13,000 L/Ha
- + Stover
- 300 kg/Ton, ~20% humidity
- + 7,000 L/ha
- ~ 20,000 L/Ha





Sources



Any lignocellulosic material, biomass from semi-arid areas

Bio-Ethanol Activities at the IBt - UNAM

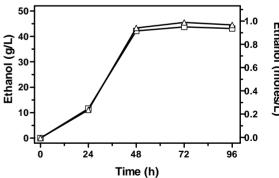


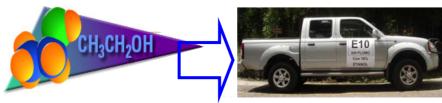
- It has a fermentation pilot plant based in 100 and 350 liters fermentors.
- We had demonstrated the generation of fermentable sugars using thermohemical and enzymatic hydrolysis at laboratory and pilot plant scale.
- We have develop (and patented) bacterial strains with the capacity to ferment all sugars present in hydrolyzates with conversions yields above 90% of the theoretical and with volumetric productivities reaching 1 g/L/h.



- Other raw materials
- Improve and integrate a process
- Cost reduction









Technological goals

- 1. Many opportunities remains to optimize ethanologenic biocatalyst
- Raw materials (lignocellulose) is different for each country or region. So process development is case specific.
- 3. Thermochemical (pre-treatments and distillation) need to be energy efficient
- 4. Enzymatic hydrolysis of cellulose needs to be optimized

Wyman. Trends in Biotechnol. 2007.

My vision:

Alfredo Martínez 2006

- Politics are very important. Biomass production is fundamental. We need to avoid competence with food and feed, and take care of land usage. Sustainable methodologies are essential for all the chain process.
- BUT DEVELOPING COUNTRIES ALSO CAN DEVELOP THEIR OWN TECHNOLOGIES, WE DO NOT NEED TO WAIT FOR THE BIG COMPANIES TO DEVELOP THEM AND LATER DEPEND ON THEM. BIOTECHNOLOGY IS FUNDAMENTAL FOR THIS TECHNOLOGIES.



!!Thanks!!



Acknowledgments

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- Estado de Morelos 2004-C02-48
 - •PAPIIT DGAPA UNAM IN220908-3

Collaborations

Instituto de Biotecnología University of Florida

Students









Production Cost and Energy Balance

Table 2. Ethanol costs and energy balances.

Feedstock	Cost (US\$ per gallon)	Energy balance (renewable output to fossi, input)
Sugarcane, Brazil		10.2 (18)
2006, without import tax	0.81 (17)	
2006, with U.S. import tax	1.35 (<i>9</i> , <i>17</i>)	
Sugar beet, Europe, 2003	2.89 (1 <i>7</i>)	2.1 (<i>19</i>)
Corn, U.S., 2006	1.03 (<i>17</i>)	1.4 (9, 11)
Cellulose ethanol, U.S.		10.0 (11)
Achieved in 2006	2.25 (11)	
Target for 2012	1.07 (11)	

Estimated Production Costs

Fuel Ethanol (dol/gal) Pesos/Liter

NREL-DOE Corn Stover: 1.44 4.20

NREL-California Lumber: 1.07 3.10

Sugar Cane Bagasse Mexico

Production Cost \$3.7 / Liter From Molasses (2001) Production Cost \$2.3 /Liter Cabrera, Gómez & Quintero 2001

Brazil Prices March 2005

(\$/L) (R/L)

Alcohol: 5.9 1.3

Gasoline: 10.4 2.3









Bio-ethanol: Mexico

Sugar Cane

- ■Planta Sn. Juan Bautista Tuxtepec (Tuxtepec, Oaxaca)
- ■Planta Tecnol del Sureste S.A de C.V (Huehuetan, Chiapas)■Ingenio La Gloria (Veracruz)

Corn

- □ Planta Mex-Starch (Sinaloa)
- □Planta Destilmex (Navolato, Sinaloa)

Sorgum

■Bioenergéticos Mexicanos S.A.P.I. de C.V (Valle Hermoso, Tamaulipas)

Cianobacterias

BioFields (Sonora

Lignocellulose

Planta Piloto IBt - UNAM



